

DETERMINATION OF THE INFLUENCE FACTORS IN DUST EXPLOSION VIA ROUGH SET: AN APPLICATION ON SYSTEM CONTROL

Yunting Tsai¹, Meili You², and Chi-Min Shu^{3*}

ABSTRACT

With the growing evolution of the chemicals and materials, the steps of chemical process have become increasingly complicated and sophisticated. There is a concern that treated dust of sugar, when produced on an industrial scale, will result in serious explosion accidents. There include test of explosion sensitivity and data processing by minimum ignition energy tester (MIET) and rough set, respectively. Five important factors of explosion discussed in dust of sugar are particle size, particle composition, temperature, as well as the relative humidity of environment. The orders of significance are particle concentration > temperature > particle size > humidity. The temperature explosive range of powdered sugar is about 19°C, and it will explode when the humidity is between 55% and 75%. When the particles of dust trend to minimum, the more amount of dust is required.

Keywords: Chemical process, explosion accidents, minimum ignition energy tester (MIET), rough set, important factors of explosion.

1. INTRODUCTION

In recent years, dust explosion hazard is always abominable, as well as an urgent problem of solution. On February 07, 2008, there are a series of sugar dust explosion at imperial sugar manufacturing facility in Port Wentworth, Georgia, and USA. (Vorderbrueggen 2001; Chang and Lin 2006). The colored powder disaster happened in new Taipei city resulting in 527 people injured (Liaw 2016). Under certain conditions, sugar can cause a dust explosion hazard. Some internal and intrinsic factor may affect the explosion properties of dust, not determining by a single factors. Therefore, all factors may affect the experiment that should be listed and analyzed the correlation between each other. Hence, we attempted to combine academic research with industrial demand and actively seek process safety and hazards elimination to reach zero disaster and business continuity (Chiu *et al.* 2016; Hajime *et al.* 2016).

The main influence features of dust explosion and features can be summarized as follows (Eckhoff 2003).

1. Chemical properties of the dust: The size of the amount of gas generated from the oxidation reaction, the size of the combustion heat, the heat generation rate and gases, all are relevant to the strength of the explosion.
2. The distribution of the size and degree of dispersion particle:

After a period of time being proceeded, the dust in the air will subside naturally. It is generally believed that particle size is between 10 to 200 μm . However, there is large difference of a variety of dust, whereby the same reasons vary depending on explosive dust particle sizes.

3. Flammable gas: In the mixing system, since the initial temperature, the system pressure, the content of the inert medium, floating in space and the wall material and the size of the ignition energy hybrid system all can make explosive limit change.
4. Temperature: Explosion limit data are related to the initial temperature of the mixture. The higher the initial temperature, the more likely the reaction tends to cause diffusion.
5. Concentration of oxygen: The higher the concentration of oxygen, the dust more easy to explode. Therefore, to reduce the concentration of oxygen, then, it can increase the lower limit of dust explosion and prevent the explosion of dust.
6. Pressure: When system pressure increases, the explosion limit range has expanded and upper explosive limit will increase. It is mainly due to the pressure rise, so that molecules move closer distance, increasing the probability of collision to make the combustion reaction easier. The explosion limits expand, especially the upper explosive limit significantly improves. When the pressure decreases, the explosion limits shrink. When the pressure falls below a certain value, the upper and lower limits will eventually overlap. At this point, the pressure is called the critical pressure of the mixed system, which is below the critical pressure, and the system will not explode.
7. Ignition strength: The higher intensity of ignition energy, the more wide-spread concentration range of spontaneous combustion is. Especially, the upper explosive limit will be moved toward a higher gas content direction.
8. Humidity: Generally speaking, combustible gas mixture of air and relative humidity have negligible impact on the width of the explosion, However, when it is extremely dry, the corresponding explosive range will be expanded.

Manuscript received June 24, 2018; revised August 28, 2018; accepted September 29, 2018.

¹ Lecturer, Center for Process Safety and Industrial Disaster Prevention, National Yunlin University of Science and Technology, Douliu, Yunlin, Taiwan 64002, R.O.C.

² Professor, Department of General Education Center, Chienkuo Technology University, 1, Chieh Shou N. Rd., Changhua, Taiwan 50094, R.O.C. Department of Safety, Health, and Environmental Engineering.

^{3*} Professor (corresponding author), Center for Process Safety and Industrial Disaster Prevention, National Yunlin University of Science and Technology, Douliu, Yunlin, Taiwan 64002, R.O.C. (e-mail: shucm@yuntech.edu.tw).

Sugar dust is tested by minimum ignition energy tester (MIEA) and discussed itself required minimum ignition energy system with different practical size and amount, temperature, and humidity, finding the crucial influence factor of dust explosion (Callé *et al.* 2005; Wu and Wu 2008).

In 1982, Professor Z. Pawlak (Pawlak 1982) presented the basic concept of rough set theory, which is based on the difference between upper approximation and lower approximation in the function of classification (Wen and Lee 2012). Meantime, the rough set theory has found plenty of real-life applications, such as in medical data analysis, finance, banking, engineering, voice recognition, image processing, and others (Kuncheva 1992; Maji and Roy 2002). The actual measurement data combined with the rough set theory analyzed the impact of dust explosion influence factors. This paper also analyzed and simulated the relationship of each relevant factor to infer the characteristics and composition of the sample, and predict explosion safety threshold, which can kick off effective early warning systems.

2. EXPERIMENTAL STUDY OF THE DUST EXPLOSION

2.1 Sample

Dust with powdered sugar was used as the object of explosion. Here the powdered sugar (sucrose) was directly obtained from the market. We used screen mesh with four different scale, > 420, 420 ~ 210, 210 ~ 105, and < 105 μm, to classify out samples.

2.2 Research Methods and Framework

The previous studies indicated seven factors influenced dust explosion, based on MIET as used in this article, a total of five quantifiable factors were established. Corresponding analytical mathematical methods can be made, and then the computer toolbox is used to analyze the weighting of each influence factor. The overall framework was shown in Fig. 1.

2.3 Minimum Ignition Energy

The equipment is shown in Figs. 2 and 3 (van den Bulck 2005; Wu and Wu 2008; Cesana and Siwek 2016; Tsai *et al.* 2018). It links existing hardware circuit, and a practical instrument to streamline the way, which is a complete analysis of the nature of the material, requiring minimum ignition energy detection circuit.

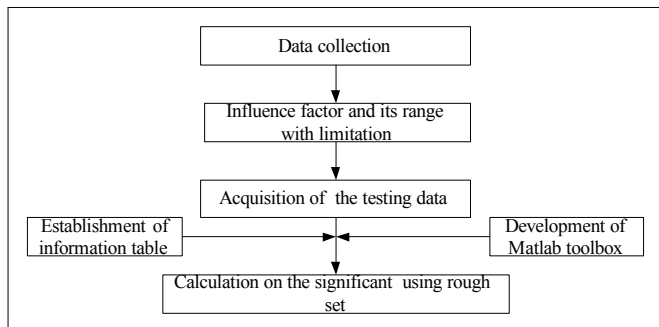


Fig. 1 Whole structure of the research flow chart

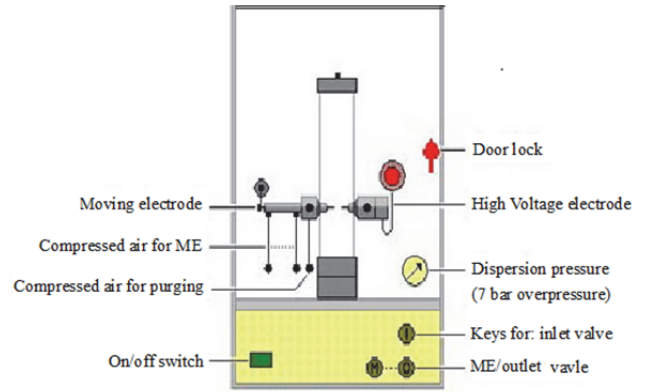


Fig. 2 Front view of MIET



Fig. 3 Outlook of MIET

2.4 Mathematics Model

The analysis steps of rough set are listed below (You and Wen 2013).

1. Information system
 $IS = (U, A)$ is called information system, where $U = \{x_1, x_2, x_3, \dots, x_n\}$ is the universe finite set of object and, $A = \{a_1, a_2, a_3, \dots, a_m\}$ is the set of attribute.
2. Information Function
 If there exist a mapping $f_a: U \rightarrow V_a$, then V_a is the set of value of a , called the domain of attribute a .
3. Discrete calculation
 The mathematics model is defined as

$$t = \frac{V_{\max} - V_{\min}}{k} \tag{1}$$

where V_{\max} : Maximum value in the data. V_{\min} : Minimum value in the data.

According to the results, we can acquire the intervals corresponding to attribute value as follows.

$$\{[d_0, d_1], [d_1, d_2], \dots, [d_{k-1}, d_k]\} \tag{2}$$

where: $d_0 = V_{\min}$, $d_k = V_{\max}$, $d_{i-1} < d_i$, $i = 1, 2, 3, \dots, k$, k is the grade of discrete.

4. Lower approximations and upper approximations
 If $A \subseteq U$, then the lower approximations and the upper approximations are defined as

$$\underline{R}(A) = \{x \in U \mid [x]_R \subseteq A\} = \bigcup \{[x]_R \in \frac{U}{R} \mid [x]_R \subseteq A\},$$

$$[x]_R = \{y \mid xRy\} \tag{3}$$

$$\overline{R}(A) = \{x \in U \mid [x]_R \cap A \neq \emptyset\}$$

$$= \bigcup \{[x]_R \in \frac{U}{R} \mid [x]_R \cap A \neq \emptyset\}, [x]_R = \{y \mid xRy\} \tag{4}$$

In other words, the lower approximation of a set is the set of all elements that surely belongs to U , whereas the upper approximation of U is the set of all elements that possibly belongs to U

- 5. Indiscernibility: An indiscernibility relation is defined as for any x_i and x_j , if x_i is identical to x_j , then x_i and x_j have all the same properties
- 6. Positive, negative and boundary: Based on the mentioned above, the positive, negative, and boundary are defined as

$$pos_R(X) = \underline{R}(X), neg_R(X) = U - \overline{R}(X), bn_R(A)$$

$$= (A) - \overline{R}(A) \tag{5}$$

- 7. Dependents: The dependents of attributes is defined as

$$\gamma_c(D) = \frac{|pos_c(D)|}{U} \tag{6}$$

Means, under $a \in C$, the ratio is in the whole set.

- 8. Significance: Under $S = (U, C \cup D, V, f)$ and $a \in C$, the significant value of attributes is defined as

$$\sigma_{(c,D)}(a) = \frac{\gamma_c(D) - \gamma_{c-\{a\}}(D)}{\gamma_c(D)} \tag{7}$$

3. RESULTS AND DISCUSSION

According to the construction information table, and using the soft-computing method by the rough set, we can analyze the weighting of influence factors to explosion (Wen et al. 2010; Tsai et al. 2018; Tsai et al. 2018; Yang et al. 2018).

- 1. Based on the state of the actual test, since the oxygen concentration is fixed, four factors were selected by using MIET results, as presented in Table 1.
- 2. According to the definition of rough set, we must first make discrete logarithm value. Since the data in particle size and particle concentration are in discrete state, according to the characteristics of temperature and humidity, this study used a quartered discrete. The discrete values are given in Table 2. In addition, we also analyzed the discrete of influence factors without non-explosion shown in Table 3.

Table 1 Five analysis factors for MIET results

| Number of factor | Particle size/ μm | Particle composition/mg | Temperature/ $^{\circ}\text{C}$ | Relative humidity/% | Experimental energy/mJ | With or without explosion? |
|------------------|------------------------------|-------------------------|---------------------------------|---------------------|------------------------|----------------------------|
| 01 | >420 | 1,200 | 20.7 | 55 | 300 | Yes |
| 02 | >420 | 1,200 | 20.7 | 56 | 100 | Yes |
| 03 | >420 | 1,200 | 18.4 | 61 | 30 | No |
| 04 | >420 | 900 | 18.5 | 66 | 300 | Yes |
| 05 | >420 | 900 | 19.0 | 65 | 100 | Yes |
| 06 | >420 | 900 | 17.3 | 61 | 30 | No |
| 07 | >420 | 600 | 19.3 | 63 | 300 | Yes |
| 08 | >420 | 600 | 19.4 | 63 | 100 | Yes |
| 09 | >420 | 600 | 17.3 | 61 | 30 | No |
| 10 | 420 ~ 210 | 1,200 | 19.8 | 73 | 300 | Yes |
| 11 | 420 ~ 210 | 1,200 | 19.6 | 72 | 100 | Yes |
| 12 | 420 ~ 210 | 1,200 | 20.1 | 72 | 30 | No |
| 13 | 420 ~ 210 | 900 | 19.6 | 72 | 300 | Yes |
| 14 | 420 ~ 210 | 900 | 19.9 | 71 | 100 | No |
| 15 | 420 ~ 210 | 900 | 20.2 | 71 | 30 | No |
| 16 | 420 ~ 210 | 600 | 19.8 | 73 | 300 | Yes |
| 17 | 420 ~ 210 | 600 | 19.8 | 72 | 100 | No |
| 18 | 420 ~ 210 | 600 | 20.1 | 71 | 30 | No |
| 19 | 210 ~ 105 | 1,200 | 20.9 | 66 | 300 | Yes |
| 20 | 210 ~ 105 | 1,200 | 20.8 | 66 | 100 | Yes |
| 21 | 210 ~ 105 | 1,200 | 20.6 | 67 | 30 | No |
| 22 | 210 ~ 105 | 900 | 20.9 | 66 | 300 | Yes |
| 23 | 210 ~ 105 | 900 | 20.9 | 66 | 100 | No |
| 24 | 210 ~ 105 | 900 | 20.9 | 66 | 30 | No |
| 25 | 210 ~ 105 | 600 | 19.8 | 69 | 300 | Yes |
| 26 | 210 ~ 105 | 600 | 20.0 | 70 | 100 | Yes |
| 27 | 210 ~ 105 | 600 | 20.8 | 69 | 30 | No |
| 28 | < 105 | 1,200 | 20.8 | 65 | 300 | Yes |
| 29 | < 105 | 1,200 | 20.8 | 66 | 100 | Yes |
| 30 | < 105 | 1,200 | 20.8 | 67 | 30 | No |
| 31 | < 105 | 900 | 20.8 | 70 | 300 | Yes |
| 32 | < 105 | 900 | 20.8 | 70 | 100 | Yes |
| 33 | < 105 | 900 | 20.7 | 67 | 30 | No |
| 34 | < 105 | 600 | 21.3 | 75 | 300 | Yes |
| 35 | < 105 | 600 | 21.1 | 71 | 100 | No |
| 36 | < 105 | 600 | 20.9 | 70 | 30 | No |

3. Substituting the data in Tables 2 and 3 into rough set equations and verified through toolbox, the significance of influence factors are shown in Fig. 4 and Table 4 (Wen and You

2016). In addition, the significance of influence factors with non-explosion are shown in Fig. 5 and Table 5.

Table 2 Four grades discrete of influence factors

| Number of factor | Particle size/ | Particle composition | Temperature | Relative humidity | Experimental energy |
|------------------|----------------|----------------------|-------------|-------------------|---------------------|
| 01 | 4 | 3 | 1 | 1 | 3 |
| 02 | 4 | 3 | 1 | 1 | 2 |
| 03 | 4 | 3 | 1 | 1 | 1 |
| 04 | 4 | 2 | 1 | 1 | 3 |
| 05 | 4 | 2 | 1 | 2 | 2 |
| 06 | 4 | 2 | 1 | 2 | 1 |
| 07 | 4 | 1 | 1 | 1 | 3 |
| 08 | 4 | 1 | 1 | 1 | 2 |
| 09 | 4 | 1 | 1 | 1 | 1 |
| 10 | 3 | 3 | 2 | 3 | 3 |
| 11 | 3 | 3 | 2 | 3 | 2 |
| 12 | 3 | 3 | 3 | 3 | 1 |
| 13 | 3 | 2 | 2 | 3 | 3 |
| 14 | 3 | 2 | 3 | 3 | 2 |
| 15 | 3 | 2 | 3 | 3 | 1 |
| 16 | 3 | 1 | 2 | 3 | 3 |
| 17 | 3 | 1 | 2 | 3 | 2 |
| 18 | 3 | 1 | 3 | 2 | 1 |
| 19 | 2 | 3 | 3 | 2 | 3 |
| 20 | 2 | 3 | 3 | 2 | 2 |
| 21 | 2 | 3 | 3 | 2 | 1 |
| 22 | 2 | 2 | 3 | 2 | 3 |
| 23 | 2 | 2 | 3 | 2 | 2 |
| 24 | 2 | 2 | 3 | 2 | 1 |
| 25 | 2 | 1 | 3 | 2 | 3 |
| 26 | 2 | 1 | 3 | 2 | 2 |
| 27 | 2 | 1 | 3 | 2 | 1 |
| 28 | 1 | 3 | 3 | 2 | 3 |
| 29 | 1 | 3 | 3 | 2 | 2 |
| 30 | 1 | 3 | 3 | 2 | 1 |
| 31 | 1 | 2 | 3 | 3 | 3 |
| 32 | 1 | 2 | 3 | 3 | 2 |
| 33 | 1 | 2 | 3 | 2 | 1 |
| 34 | 1 | 1 | 3 | 3 | 3 |
| 35 | 1 | 1 | 3 | 3 | 2 |
| 36 | 1 | 1 | 3 | 3 | 1 |

Table 3 Four grades discrete of influence factors without non-explosion

| Number of factor | Particle size | Particle composition | Temperature | Relative humidity | Experimental energy |
|------------------|---------------|----------------------|-------------|-------------------|---------------------|
| 01 | 4 | 3 | 1 | 1 | 2 |
| 02 | 4 | 3 | 2 | 1 | 1 |
| 04 | 4 | 2 | 1 | 1 | 2 |
| 05 | 4 | 2 | 1 | 2 | 1 |
| 07 | 4 | 1 | 2 | 1 | 2 |
| 08 | 4 | 1 | 2 | 1 | 1 |
| 10 | 3 | 3 | 2 | 3 | 2 |
| 11 | 3 | 3 | 2 | 3 | 1 |
| 13 | 3 | 2 | 2 | 3 | 2 |
| 16 | 3 | 1 | 2 | 3 | 2 |
| 19 | 2 | 3 | 3 | 2 | 2 |
| 20 | 2 | 3 | 3 | 2 | 1 |
| 22 | 2 | 2 | 3 | 2 | 2 |
| 25 | 2 | 1 | 2 | 2 | 2 |
| 26 | 2 | 1 | 3 | 2 | 1 |
| 28 | 1 | 3 | 3 | 2 | 2 |
| 29 | 1 | 3 | 3 | 2 | 1 |
| 31 | 1 | 2 | 3 | 3 | 2 |
| 32 | 1 | 2 | 3 | 3 | 1 |
| 34 | 1 | 1 | 3 | 3 | 2 |

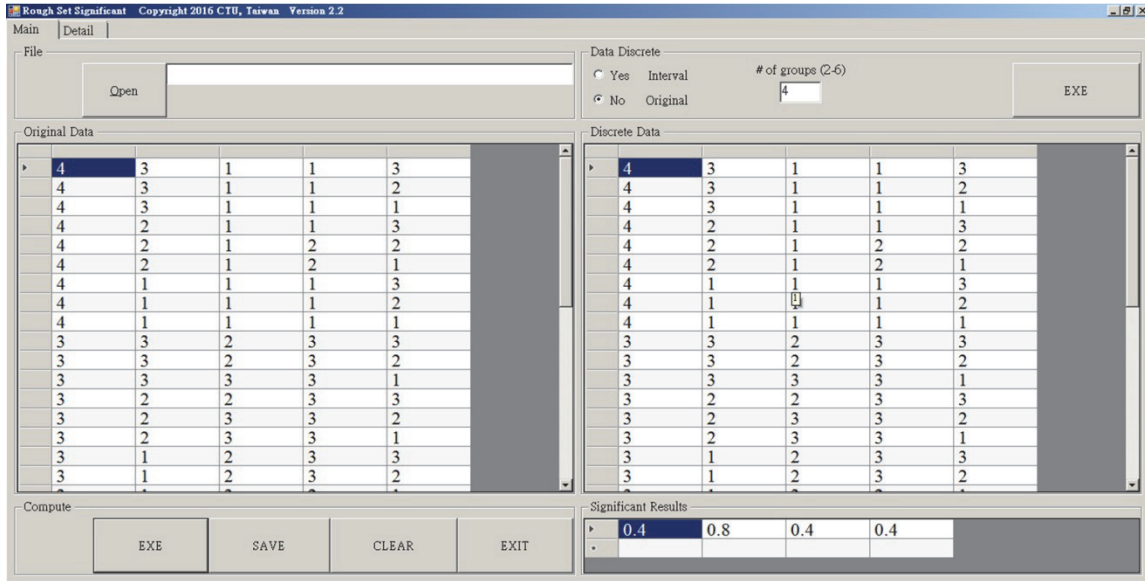


Fig. 4 Verification using toolbox

Table 4 Significance of influence factors fewer than four grades

| Factor | Particle size | Particle composition | Temperature | Relative humidity |
|-----------------------|---------------|----------------------|-------------|-------------------|
| Weighting of 4 grades | 0.4 | 0.8 | 0.4 | 0.4 |

Table 5 Significance of influence factors under four grades without non-explosion

| Number of factor | Particle size | Particle composition | Temperature | Relative humidity |
|-----------------------|---------------|----------------------|-------------|-------------------|
| Weighting of 4 grades | 0 | 0.6 | 0.4 | 0.2 |

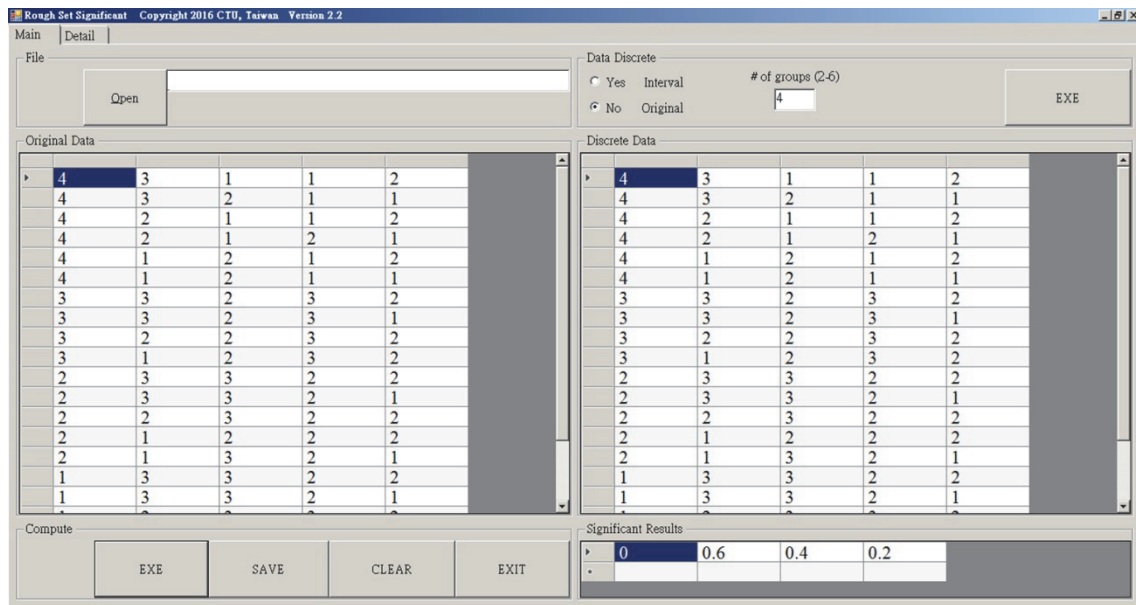


Fig. 5 Verification using toolbox without non-explosion

Through the calculation results from rough set, we can draw conclusions into two parts:

1. No matter what the state is in exploration state or non-explosion state, about the influence factors, the

weighting of particle composition was 0.8, and the weighting of particle size, temperature and humidity all reached 0.4, it can receive that the weighting of particle concentration is two times of the other three factors obviously.

2. Under the explosion state, the weighting of particle composition was 0.6, the weighting of temperature was 0.4, the weighting of humidity was 0.2, and particle size seems did not have any influence in exploration.

4. CONCLUSIONS

Since dust explosion cases often occur among life, and powdered sugar is often used in our daily life (i.e., bakery shops and food manufactures), this paper used powdered sugar as tested substances. The minimum ignition energy was imposed high-voltage tester to make the powdered sugar reach explosion energy, and then the impact of environmental factors on powdered sugar can be identified. Through the actual test and the rough set analysis, the order of importance of the influence factors can be listed as follows: Particle concentration > temperature > particle size > humidity, which is in good agreement with actual situation. The temperature explosive range of powdered sugar is about 19 degrees Celsius, and it will explode when the humidity is between 55% and 75%. When particles reach their minimum, if the amount is not enough, it will no long explode. However, the biggest reason influence the state of substances is temperature. This can be learned from Formosa Fun Coast Water Park explosion in new Taipei city, Taiwan, which happened in summer, 2014.

In this article, the subject was only powdered sugar. In the future, it is suggested to extend to other materials, such as corn flour, wheat flour, and cornstarch. Furthermore, the difference of oxygen, such as 21%, 16%, and 12%, can test and analyze the oxygen's impact on explosion. In addition, except using rough set theory, other soft-computing methods can also be used, like the grey system theory and the fuzzy theory, to make cross-comparison. It is believed that more convincing and feasible results can be reached.

ACKNOWLEDGEMENTS

Financial support for this study was graciously provided by Chang Chun Group (CCPG), and Ministry of Education, Taiwan, R.O.C.

REFERENCES

- Callé, S., Klabá, L., Thomas, D., Perrin, L., and Dufaud, O. (2005). "Influence of the size distribution and concentration on wood dust explosion: Experiments and reaction modeling." *Powder Technology*, **157**, 144-148.
- Cesana, C. and Siwek, R. (2016). *Powder Explorer Manual*. Swiss.
- Chang, J.I. and Lin, C.C. (2006). "A study of storage tank accidents." *Journal of Loss Prevention in the Process Industries*, **19**, 51-59.
- Chiu, Y.C., Hong, W.T., and Chen, N. (2016). "Ultrasonically dispersed dyed water mists as a substitute for colored powders." *Case Studies in Fire Safety*, **6**, 1-9.
- Eckhoff, R.K. (2003). *Dust Explosions in the Process Industries*. Gulf professional publishing of Elsevier Science, New York, U.S.A.
- Hajime, M., Nobuyuki, H., and Hiroto, I. (2016). "First experience using cultured epidermal autografts in Taiwan for burn victims of the Formosa Fun Coast Water Park explosion, as part of Japanese medical assistance." *Burns*, **42**, 697-703.
- Kuncheva, L.I. (1992). "Fuzzy rough sets: Application to feature selection." *Fuzzy Sets and Systems*, **51**, 147-153.
- Liaw, H.J. (2016). "Lessons in process safety management learned in the Kaohsiung gas explosion accident in Taiwan." *Process Safety Progress*, DOI: 10.1002/prs.11818.
- Maji, P.K. and Roy, A.R. (2002). "An application of soft sets in a decision making problem." *Computers & Mathematics with Applications*, **44**, 1077-1083.
- Pawlak, Z. (1982). "Rough sets." *Journal Computer Information Science*, **11**, 341-356.
- Tsai, Y.T., Huang, A.C., Ho, S.C., and Shu, C.M. (2018). "Potential explosion hazard of polyester resin dust formed from a granulation process: Limiting oxygen concentration with different pressures." *Applied Thermal Engineering*, **135**, 74-82.
- Tsai, Y.T., Liao, J.Y., Shu, C.M., 2018. "Explosion characteristics of chlorodifluoromethane and isobutane at high temperature and pressure using a 20-L apparatus." *International Journal of Refrigeration*, **96**, 155 -160.
- Tsai, Y.T., Yang, Y.C. Wang, C., Shu, C.M., and Deng, J. (2018). "Comparison of the inhibition mechanisms of five types of inhibitors on spontaneous coal combustion." *International Journal of Energy Research*, **42**, 1158-1171.
- van den Bulck, E. (2005). "Closed algebraic expressions for the adiabatic limit value of the explosion constant in closed volume combustion." *Journal of Loss Prevention in the Process Industries*, **18**, 5-42.
- Vorderbrueggen, J.B. (2001). "Imperial sugar refinery combustible dust explosion investigation." *Process Safety Progress*, **30**, 66-81.
- Wen, K.L. and Lee, Y.T. (2012). "Apply rough set theory in the function group analysis for phenolic amide compounds." *Computers and Electrical Engineering*, **38**, 11-18.
- Wen, K.L. and You, M.L. (2016). *Data Mining in the Applications of Big Data*, Taiwan Kansei Information Association, Taichung.
- Wen, K.L., Nagai, M., Chao, J.S., Chen, H.Y., and Wang, X. (2010). *The Basic Concept of Rough Set Theory and Matlab GUI Toolbox*. Taiwan Kansei Information Association, Taichung.
- Wu, H.J. and Wu, C.W. (2008). *Study of Explosion Characteristics of Industrial Nano Dust Used in Domestic*. Institute of Labor, Occupational Safety and Health, Taipei, Taiwan.
- Yang, Y., Tsai, Y.T., Zhang, Y., Shu, C.M. and Deng, J. (2018). "Inhibition of spontaneous combustion for different metamorphic degrees of coal by Zn/Mg/Al-CO₃-layered double hydroxide." *Process Safety and Environmental Protection*, **113**, 401-412.
- You, M.L. and Wen, K.L. (2013). "Application of rough set method to the weightings of high temperature creep factors of boiler water wall." *Proceedings of IEEE/SICE International Symposium on System Integration*, 729-734, Kobe, Japan.